

1 **Energetics of a bouncing drop: coefficient of restitution, bubble entrapment and**  
2 **escape**

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8 Drops bouncing on an ultra-smooth solid surface can either make contact with the sur-  
9 face or be supported on a thin cushion of gas. If the surface is superhydrophobic, either  
10 complete or partial rebound usually occurs. Recent experiments have shed light on the  
11 lubrication effect of the underlying gas layer at the onset of impact. Using axisymmetric  
12 direct numerical simulations, we shed light on the energetics of a drop bouncing from a  
13 solid surface. A complete energy budget of the drop and the surrounding gas during one  
14 complete bouncing cycle reveals complex interplay between various energies that occur  
15 during impact. Using a parametric study, we calculate the coefficient of restitution as a  
16 function of Reynolds and Weber numbers and the results are in good agreement with re-  
17 ported experiments. Our simulations reveal that Weber number and not Reynolds number  
18 has a stronger effect on energy losses as the former affects the shape of the drop during  
19 impact. At higher Weber and Reynolds numbers, a tiny gas bubble gets trapped inside the  
20 drop during impact. We show that a large amount of dissipation occurs during bubble en-  
21 trapment and escape process. Finally, analysis of the flow field in the underlying gas layer  
22 reveals that maximum dissipation occurs in this layer and a simple scaling law is derived  
23 for dissipation that occurs during impact.

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## 25 I. INTRODUCTION

26 Understanding the dynamics of drop impact near a solid surface offers insights into a diverse  
27 range of applications ranging from ink-jet printing<sup>1,2</sup> to heat transfer through spray cooling<sup>3</sup>. Ex-  
28 cellent reviews by Yarin<sup>4</sup> and Josserand & Thoroddsen<sup>5</sup> cover many aspect of drop impact dynam-  
29 ics. In the last two decades a number of new and surprising discoveries have been made starting  
30 with the seminal work of Xu *et al.*<sup>6</sup> who showed that pressure of the surrounding gas plays a cru-  
31 cial role during the splashing process. This discovery prompted Mandre *et al.*<sup>7</sup> and Mani *et al.*<sup>8</sup>  
32 to develop a theory to examine the role of gas and lubrication effects near the solid surface at the  
33 onset of impact. Experiments by Kolinski *et al.*<sup>9</sup> indeed found that drop tends to skate on a thin  
34 layer of gas before touchdown. Another important discovery made in recent years is that drops can  
35 bounce on a smooth surface without ever making contact with it<sup>10,11</sup>. A thin layer of gas cushions  
36 the impact and lubrication pressure provides the necessary repulsion force for the drop to bounce  
37 back. Using interferometric techniques, de Ruiter *et al.*<sup>11,12</sup> characterised the gas film beneath the  
38 drop in great detail and showed that gas films of thickness in the micrometer and nanometer range  
39 is trapped beneath the drop.

40 In a companion paper, we recently conducted an exhaustive numerical study of a drop im-  
41 pacting a solid surface assuming the gas to be incompressible<sup>13</sup> and key results of this work is  
42 briefly summarized below. Through a parametric study, the simulations revealed that wettability-  
43 independent (WI) or non-contact bouncing and wettability-dependent (WD) or bouncing with con-  
44 tact are separated by a transition boundary in the  $We - Re$  plane. The simulations also revealed  
45 that WI bouncing is favoured at low  $Re$  for a wide range of Weber numbers. In such cases, the drop  
46 spreads on a thin layer of gas beneath it. Kolinski *et al.*<sup>10</sup> noted that large shear rates generated  
47 in this gas layer can lead to excessive dissipation reducing the coefficient of restitution, always  
48 below 0.65 in their experiments, in spite of the low viscosity of air. In contrast, Richard & Quéré<sup>14</sup>  
49 report a coefficient of restitution close to 0.9 for a drop bouncing on a superhydrophobic surface.  
50 Such a large value in their experiments was attributed to very short contact times during which  
51 dissipation is negligible. The results of Kolinski *et al.* is also in contrast to similar experiments by  
52 de Ruiter *et al.*<sup>11</sup> who reported a very high coefficient of restitution of  $0.96 \pm 0.04$ . Using careful  
53 estimation of the energy budget for a wide range of  $We$  and  $Re$ , we show later that the apparent

54 discrepancy in the coefficient of restitution between Kolinski *et al.*<sup>10</sup> and de Ruiter *et al.*<sup>15</sup> can be  
55 resolved by examining the role of Weber and Reynolds numbers. To determine the coefficient of  
56 restitution ( $r_c$ ) accurately, it is necessary to precisely compute the energy budget of a drop during  
57 a bouncing event. Closely connected to  $r_c$  is the contact time,  $\tau$ , which is defined as the duration  
58 for which the drop stays in *contact* with the solid surface.

59 For water drops of about 1 mm at moderate impact velocities typically in the range of 0.2 to 2  
60 m/s, Richard *et al.*<sup>16</sup> show that contact time scales with radius of the drop as  $\tau \sim R^{3/2}$ , obtained  
61 by balancing inertia of the drop with surface tension and is independent of velocity. Okumura  
62 *et al.*<sup>17</sup> showed that drop deformation and contact time depends on a delicate balance of inertia,  
63 gravity and surface tension. At lower impact velocities, they show that contact time increases  
64 with decreasing velocity and drop deformation scales as  $We^{1/2}$ . A more sophisticated quasi-static  
65 model of drop impact was developed by Moláček & Bush<sup>18</sup> who showed that contact time and  
66 coefficient of restitution depend on both Weber and Ohnesorge numbers.

67 Understanding the energetics of drop impact also helps determine the radial extent of drop  
68 spreading upon impact. Kim & Chun<sup>19</sup> performed experiments using a variety of drop and solid  
69 combinations to study spreading and recoiling dynamics. They used an empirically determined  
70 dissipation factor to account for viscous dissipation during drop spreading and found that increas-  
71 ing Weber number promotes faster recoil. Not surprisingly, drops with large equilibrium contact  
72 angle were found to have very short contact times, a result consistent with the finding of Richard *et al.*<sup>14</sup>  
73 *et al.*<sup>14</sup>. For drops bouncing on superhydrophobic surfaces at higher Weber numbers, contact dissi-  
74 pation may be small, but such drops undergo pronounced oscillations after lift-off which generates  
75 vigorous motion inside the drop leading to additional viscous dissipation. Richard *et al.*<sup>16</sup> argue  
76 that in their experiments, bulk of the dissipation is due internal motion inside the drop caused by  
77 damped surface oscillations after lift-off. We later quantify such internal dissipation in relation to  
78 surface oscillations as a function of Weber and Reynolds numbers. Pasandideh-Fard *et al.*<sup>20</sup> de-  
79 veloped a simple model for the maximum extension diameter of the drop,  $D_{\max}$ , assuming that all  
80 the initial kinetic and surface energy is converted to surface energy and viscous dissipation when  
81 the drop spreads to its maximum extent. Their model improves upon an earlier model by Chandra  
82 & Avedisian<sup>21</sup> which overestimated the value of  $D_{\max}$ . Clanet *et al.*<sup>22</sup> performed experiments with  
83 a low-viscosity drop impacting a superhydrophobic surface for moderate values of Weber num-  
84 ber ( $2 < We < 900$ ) where  $We = \rho_l V_0^2 R_0 / \sigma$  is the Weber number associated with impact velocity  
85  $V_0 (= \sqrt{2gH_0})$  for drop of radius  $R_0$  with density and surface tension denoted by  $\rho_l$  and  $\sigma$  respec-

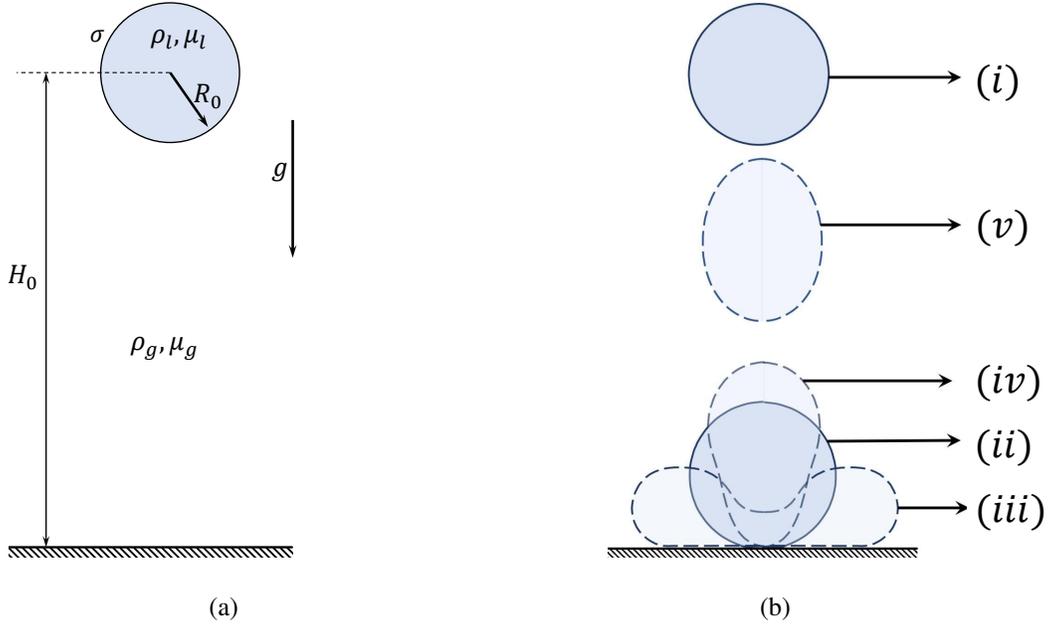


FIG. 1. (a) Schematic of the problem set-up showing all the relevant parameters in the problem. (b) Schematic view of the typical shapes assumed by the drop during one complete bouncing cycle. The solid curves (*i*, *ii*) show the shape of the drop at  $t = 0$  and at the onset of impact. The other shapes shown with dashed lines at (*iii*), (*iv*) and (*v*) correspond to shape at maximum deformation on the surface, at the instant of lift-off from the surface and at the maximum height after impact, respectively.

86 tively, and showed that  $D_{max} \sim We^{1/4}$ . This differs from the low Weber number experiments for  
 87 drops on superhydrophobic surfaces where a different scaling is observed,  $D_{max} \sim We^{1/2}$ .

88 In this study, we use direct numerical simulations to calculate the energy budget of an impact-  
 89 ing drop with emphasis on how various exchanges of energies differ as a function of Weber and  
 90 Reynolds numbers. We further show how coefficient of restitution varies with  $We$  and  $Re$  which  
 91 will help resolve the discrepancy between the values reported by de Ruiter *et al.*<sup>11</sup> and Kolinski *et*  
 92 *al.*<sup>10</sup>.

## 93 II. NUMERICAL SET-UP AND ENERGETICS

94 We numerically simulate a falling drop using the open source code *Gerris* in an axisymmet-  
 95 ric configuration. The code, developed by Popinet<sup>23</sup> uses an advanced quaternary adaptive mesh  
 96 refinement and is well known for its accurate interface capture algorithm and surface tension  
 97 implementation<sup>24</sup>. The geometry used in the current study is identical to a recently completed

98 study for drop impact on solid surface<sup>13</sup>. For suitability of the solver to drop impact dynamics and  
 99 validation studies, the reader is referred to our companion paper<sup>13</sup>.

100 A drop of radius  $R_0$  is released from an initial height  $H_0$  and a schematic of the problem set-  
 101 up is shown figure 1. The viscosity ratio between the drop and the surrounding gas is fixed at  
 102  $\mu_l/\mu_g = 55.5$  mimicking a water drop falling in air. For numerical stability, we keep the density  
 103 ratio fixed at  $\rho_l/\rho_g = 100$  though a value of 1000 showed no appreciable difference in the results.  
 104 Further, since the focus will be on collision dynamics near the solid surface, viscosity ratio plays  
 105 a more important role than density ratio. To facilitate complete rebound, the contact angle is  
 106 kept fixed at  $170^\circ$  inspired by the experiments of Richard & Quéré<sup>14</sup>. For low  $We$  and  $Re$ , drop  
 107 bounces without ever making contact with the solid surface. In such cases, the impact is cushioned  
 108 by a thin film of gas beneath the drop and is referred to as wettability-independent bouncing.  
 109 In Sharma & Dixit<sup>13</sup>, we show that the drop shapes as well as the drop-gas interface profiles  
 110 during contact are in good agreement with experiments for water in air scenario. Moreover, the  
 111 numerical results were found to be in excellent agreement with well established scaling laws for  
 112 the height of the drop when it undergoes its first deformation before impact,  $H_d \sim Ca_g^{1/2}$  derived  
 113 by Pack *et al.*<sup>25</sup>, and the minimum thickness of gas film,  $h_{min} \sim St^{-8/9}We^{-2/3}$  derived by Mandre  
 114 *et al.*<sup>7</sup> where  $St = \rho_l V_0 R_0 / \mu_g$  is the Stokes number. A phase-diagram in the  $We - Re$  plane,  
 115 shown in figure 2, shows two distinct regimes of impact referred to as wettability-independent  
 116 (WI) contact and wettability-dependent (WD) contact. In the WI regime, the drop is supported on  
 117 a thin gas layer whose thickness scales with  $We$  and  $St$ . In the WD regime, contact occurs either  
 118 at the outer periphery of the drop or near the axis of symmetry. To enable complete rebound,  
 119 all our simulations are carried out at a fixed contact angle of  $170^\circ$  representing bouncing from  
 120 superhydrophobic surfaces similar to the experiments of Richard & Quere<sup>14</sup>.

121 The primarily goal of this study is to obtain detailed energy budget as the drop completes  
 122 one bouncing cycle, i.e., drop from an initial release height  $H_0$  impacts the surface and reaches  
 123 a new height after lift-off,  $H_1$ . During this motion, potential energy of the drop,  $E_P(t)$ , converts  
 124 to kinetic and surface energies,  $E_K(t)$  and  $E_S(t)$ . Drag due to surrounding gas as well as internal  
 125 motions within the drop contributes to viscous dissipation. Let  $E_0$  be the initial energy of the drop  
 126 given by  $E_0 = E_P^{(0)} + E_S^{(0)}$ . Applying the principle of energy conservation, the drop has to obey the  
 127 following relation:

$$128 \quad E_P(t) + E_K(t) + E_S(t) + D(t) = E_0, \quad (1)$$

129 where  $D(t)$  represents viscous dissipation of energy. It is instructive to combine energies associ-

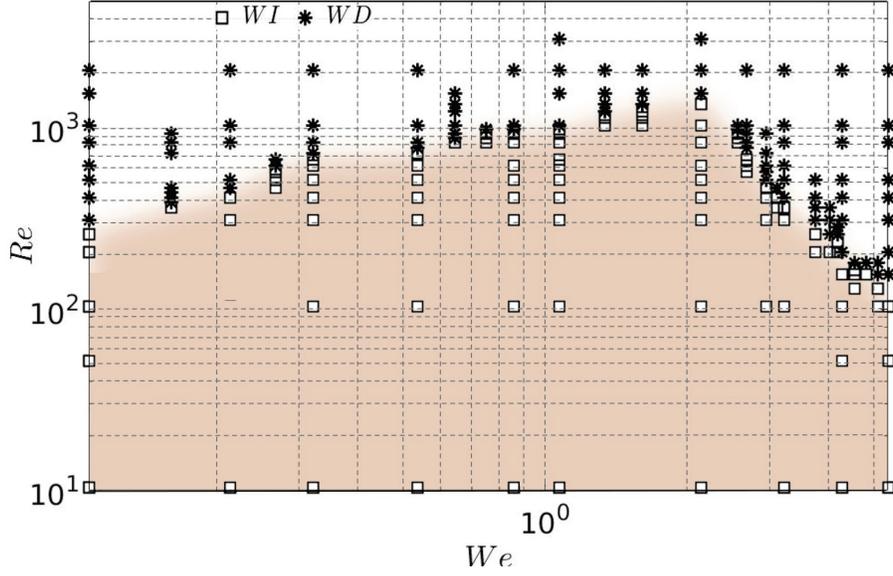


FIG. 2. Phase-diagram in the  $Re - We$  plane showing two distinct regimes, the wettability-independent regime (WI) (also shown with a shaded region) and the wettability-dependent regime (WD). The symbols correspond to parameter values where simulations are carried out for one complete bouncing cycle. The transition between the two regimes is grid dependent (see companion paper<sup>13</sup> for more details).

130 ated only with the drop to highlight the role played by the gas. We therefore define

$$131 \quad E(t) = E_P(t) + E_{K,d}(t) + E_S(t), \quad (2)$$

132 where the subscript  $d$  in the kinetic energy shows that this energy is only associated with the drop  
 133 motion. All the energies defined above can be calculated in terms of the flow fields and drop shape  
 134 numerically using the integrals

$$135 \quad E_P(t) = \int_{\Omega} \rho_l B g h d\Omega, \quad (3)$$

$$136 \quad E_{K,d}(t) = \frac{1}{2} \int_{\Omega_d} \rho_l (u^2 + v^2) d\Omega = \frac{1}{2} \int_{\Omega} \rho_l B (u^2 + v^2) d\Omega, \quad (4)$$

$$137 \quad E_{K,g}(t) = \frac{1}{2} \int_{\Omega_g} \rho_g (u^2 + v^2) d\Omega = \frac{1}{2} \int_{\Omega} \rho_g (1 - B) (u^2 + v^2) d\Omega. \quad (5)$$

138 In the above expressions,  $u$  and  $v$  are radial and axial velocities and  $B$  is the volume fraction of  
 139 liquid with  $B = 1$  representing the liquid phase and  $B = 0$  representing the gas phase. In the  
 140 volume-of-fluid method adopted in the current study, the interface cells have a value of  $B$  between  
 141 0 and 1 such that density of any cell is given by  $\rho = B\rho_l + (1 - B)\rho_g$ . When the drop is not in

142 contact with the solid surface, surface energy is simply the product of surface tension (liquid-gas  
 143 free energy,  $\sigma$ ) and surface area of the drop. But when the drop is in contact with the solid,  
 144 additional interfacial energy between the drop and the solid,  $\sigma_{sl}$ , needs to be taken into account.  
 145 For a contact angle,  $\theta = \theta_e$ , and using Young's law, the surface energy can be defined as,

$$146 \quad E_S(t) = \begin{cases} \sigma A_s(t) & \text{during flight,} \\ \sigma (A_s(t) - a_s(t) \cos(\theta_e)) & \text{during contact,} \end{cases} \quad (6)$$

147 where  $\sigma$  is the surface tension of the drop-gas interface,  $A_s(t)$  is the surface area of the drop-gas  
 148 interface and  $a_s(t)$  is the surface area of the drop-solid interface.

149 Energy lost through viscous dissipation in equn. (1) is obtained by integrating the rate of  
 150 dissipation of mechanical energy, per unit mass of the fluid, due to viscosity,  $\Phi$ , as

$$151 \quad D(t) = \int_0^t \Phi(s) ds, \quad (7)$$

152 where  $\Phi(t)$  can be written in terms of the stress tensor  $\mathbf{T}$  and rate-of-strain tensor  $\mathbf{S}$  as

$$153 \quad \begin{aligned} \Phi &= \int_{\Omega_d \cup \Omega_g} \mathbf{T} : \mathbf{S} d\Omega, \\ 154 \quad &= \int_{\Omega} \left[ 2\mu \left( \left( \frac{\partial u}{\partial r} \right)^2 + \left( \frac{\partial v}{\partial y} \right)^2 + \left( \frac{u}{r} \right)^2 \right) + \mu \left( \frac{\partial v}{\partial r} + \frac{\partial u}{\partial y} \right)^2 \right] d\Omega. \end{aligned} \quad (8)$$

155 Here  $\Omega_d$  and  $\Omega_g$  representing the drop and gas phases, respectively, and  $\mu = B\mu_l + (1 - B)\mu_g$  is  
 156 average viscosity in a cell. Since some of the drop's energy is lost to the kinetic energy of the gas,  
 157  $E_{K,g}$ , we define two new energy terms:

$$158 \quad E_D(t) = E(t) + D(t), \quad (9)$$

$$159 \quad E_T(t) = E_D(t) + E_{K,g}(t). \quad (10)$$

160 The first expression,  $E_D(t)$ , represents total energy of the drop including viscous dissipation (in  
 161 drop and gas) while the second expression,  $E_T(t)$  is the total energy of the system accounting for  
 162 all losses, thus  $E_T$  should be equal to  $E_0$  at all times. Apart from minor numerical errors,  $E_T$  is  
 163 practically indistinguishable from  $E_0$  in our simulations guaranteeing the numerical accuracy of  
 164 the solver.

165 Having defined all the relevant energy quantities, we define two new quantities to quantify  
 166 energy loss during drop impact. The total energy loss during one complete bouncing cycle, for a

TABLE I. Glossary of important parameters used in the study

Initial energy of the drop ( $t = 0$ )	$E_0 = E_P(t) + E_K(t) + E_S(t) + D(t)$	Equn. (1)
Total energy of the drop	$E(t) = E_P(t) + E_{K,d}(t) + E_S(t)$	Equn. (2)
Potential energy of the drop	$E_P(t)$	Equn.(3)
Kinetic energy of the drop	$E_{K,d}(t)$	Equn.(4)
Kinetic energy of the gas	$E_{K,g}(t)$	Equn.(5)
Surface energy of drop-gas interface	$E_S(t)$	Equn.(6)
Viscous dissipation	$D(t)$	Equn. (7)
Total energy loss	$L_T(t)$	Equn. (11)
Energy loss in contact	$L_c(t)$	Equn. (12)
Coefficient of restitution	$r_c = \sqrt{ V_1 / V_0 }$	Equn. (14)
Reynolds number	$Re$	$\frac{\rho_l V_0 R_0}{\mu_l}$
Stokes number	$St$	$\frac{\rho_l V_0 R_0}{\mu_g}$
Weber number	$We$	$\frac{\rho_l V_0^2 R_0}{\sigma}$

167 drop starting at height  $H_0$  till it again attains a new maximum height  $H_1$  after its first impact can  
 168 be calculated in terms of the total loss,  $L_T$ , defined by

$$169 \quad L_T = E_0 - E_1. \quad (11)$$

170 Similarly, loss of energy during impact can be calculated as

$$171 \quad L_c = E_b - E_a \quad (12)$$

172  $E_b$  and  $E_a$  are the total energies of the drop before (taken to be the instant of time at when the drop  
 173 undergoes its first deformation) and after impact, respectively. Table I summarizes all the energies  
 174 and parameters used in this work.

### 175 III. RESULTS AND DISCUSSION

#### 176 A. Energy budget

177 All energies are non-dimensionalized by the initial total energy,  $E_0$ , and their variation with  
 178 time is shown in figure 3 as the drop completes one complete rebound cycle for  $We = 3.21$  and

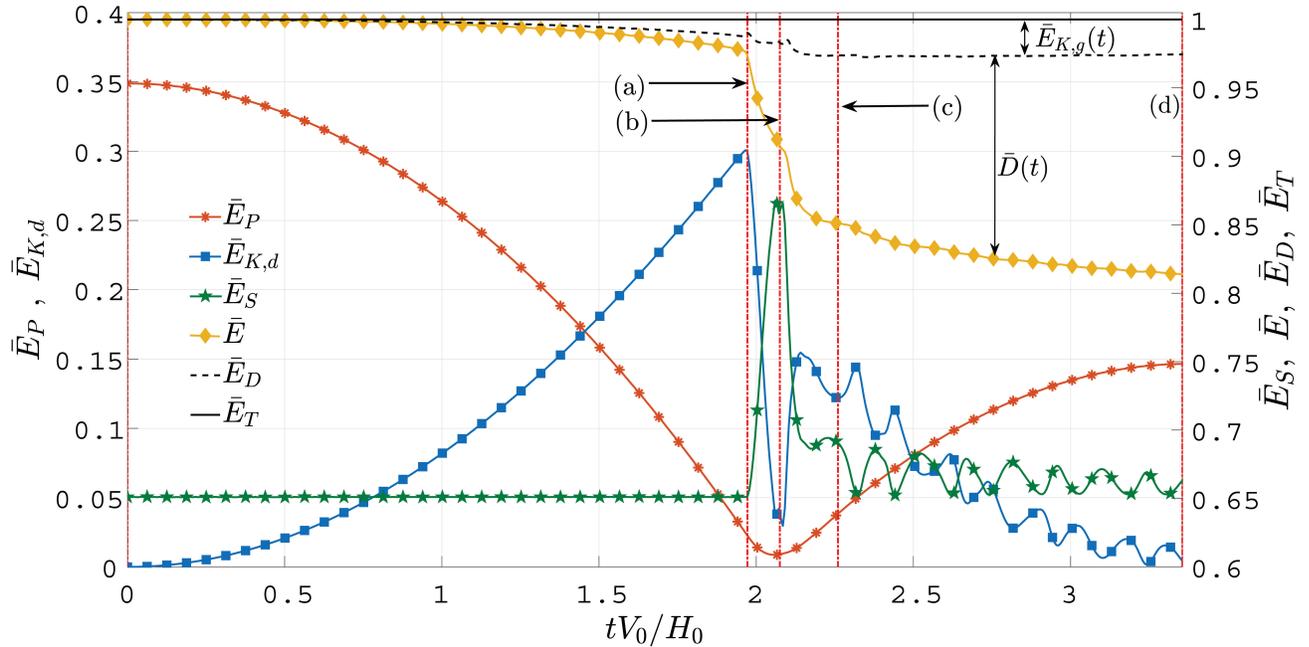


FIG. 3. Energy budget for one complete bouncing cycle for  $We = 3.21$  and  $Re = 207$  showing various energies associated with the drop and the gas non-dimensionalized with the initial energy  $E_0$ . The kinetic,  $\bar{E}_{K,d}$ , and potential energies,  $\bar{E}_P$ , are shown on the left y-axis while surface energy,  $\bar{E}_S$ , energy of the drop without viscous dissipation,  $\bar{E}$ , energy of the drop with viscous dissipation,  $\bar{E}_D$ , and total energy of the drop and gas,  $\bar{E}_T$ , are shown on the right y-axis. See text for more details. Note the difference in scale on both the y-axis. The vertical dash-dot lines shown with (a), (b), (c) and (d) represents time at the onset of impact, at maximum deformation of the drop, at the onset of lift-off and at maximum height, respectively.

179  $Re = 207$ , a case in the wettability independent regime of figure 2. Variations in energy budget  
 180 is punctuated by distinct phases in drop's evolution during the impact process which are shown  
 181 by vertical lines marked (a) through (d). The corresponding drop shapes at each of these times is  
 182 shown in figure 4. At  $t = 0$ , drop descends from rest possessing only potential and surface energy.  
 183 The ratio of these two energies is given by

$$184 \quad \frac{E_P^{(0)}}{E_S^{(0)}} = \frac{We}{6}. \quad (13)$$

186 In this particular case,  $E_S^{(0)} > E_P^{(0)}$  due to the small Weber number used. At the instant shown by  
 187 (a) in figure 3, drop begins to deform from its spherical shape indicated by a concomitant increase  
 188 in surface energy. At this instant of time, the kinetic energy of the drop is at its maximum and

189 the drop shape is shown in figure 4(a). A region of high pressure is developed beneath the drop  
 190 which rapidly decelerates the drop’s motion. The drop soon makes ‘touchdown’, but in this case,  
 191 supported on a thin cushion of gas below it. The kinetic energy of the drop then rapidly reduces  
 192 at the expense of its surface energy and the drop deforms to its maximum radial extent at time  
 193 shown by (b). The drop shape along with the pressure field inside it at this time is shown in figure  
 194 4(b). Even at the drop’s maximum extent, internal circulation does not completely cease giving  
 195 rise to a non-zero kinetic energy. In Sharma & Dixit<sup>13</sup>, we show that maximum spreading diameter  
 196 obeys the scaling,  $D_{max} \sim We^{1/2}$ . This scaling was first derived by Richard & Quéré<sup>14</sup> using the  
 197 argument of exchange of kinetic and surface energy during impact and the results in figure 3 are  
 198 consistent with their findings. Surface tension then causes the drop to retract and it eventually  
 199 achieves lift-off from the solid surface at time (c). The drop takes the shape of a distorted prolate  
 200 spheroid as shown in figure 4(c). Most of the viscous dissipation occurs during impact as evident  
 201 from a large decrease in drop’s energy,  $E(t)$ , given in equn. (2), between times (a) and (c). The  
 202 drop continues to oscillate during its ballistic motion causing additional viscous dissipation due to  
 203 internal circulation inside the drop. As a result, both kinetic and surface energy exhibit damped  
 204 oscillations providing a route for continuous loss of drop’s energy during its flight. In section IV,  
 205 we return to the issue of energy loss and compare loss during contact and during flight in greater  
 206 detail. It has to be noted that only a small fraction of the drop’s energy is exchanged with the gas,  
 207 shown as  $E_{K,g}$ , in this case, less than 2.5%. During drop’s upward motion, we observe a nearly  
 208 perfect exchange of kinetic and surface energies as shown in figure 5. To compare these energies,  
 209 we plot only the fluctuating part of the energies obtained by subtracting out the moving-average  
 210 value. The drop eventually reaches a new maxima,  $H_1$ , losing approximately 20% of its total  
 211 energy  $E_0$ , and the drop shape at the new height is shown in figure 4(d).

212 We now examine how energy budget for a falling drop changes with time for a sample case  
 213 in the wettability-dependent regime of the phase diagram 2. The energy budget with  $We = 3.21$   
 214 and  $Re = 1035$  is shown in figure 6 and has to be viewed in conjunction with evolution of drop  
 215 shapes shown in figure 7 as well as three-dimensional and streamline plots showing bubble capture  
 216 and escape shown in figures 8, 9 and 10 respectively. The evolution of all energies until the first  
 217 deformation of the drop, shown with vertical dash-dot line at (a), is identical to the previous case  
 218 at  $Re = 207$ . Inertia causes the drop to rapidly spread on the surface until time (b) when surface  
 219 energy reaches a maximum at the expense of kinetic energy. The interface at the axis of symmetry  
 220 continues to move downwards while the drop retreats inward radially. Capillary waves generated

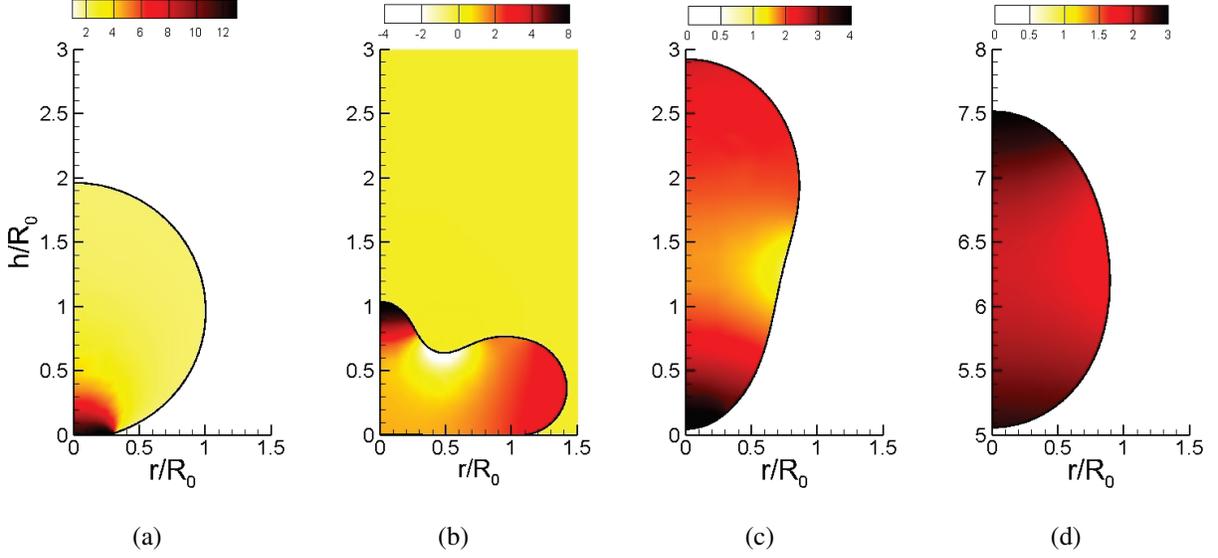


FIG. 4. Drop shapes for  $We = 3.21$  and  $Re = 207$  at four different times: (a)  $\bar{t} = 1.9719$ , (b)  $\bar{t} = 2.075$ , (c)  $\bar{t} = 2.26$  and (d)  $\bar{t} = 3.349$ . The colour contours show the variation of non-dimensional pressure,  $\bar{P} = P/(\sigma/R_0)$ . The four panels corresponding to time instants shown with vertical dash-dot lines in the energy budget 3. Note that contour levels are different in the four panels.

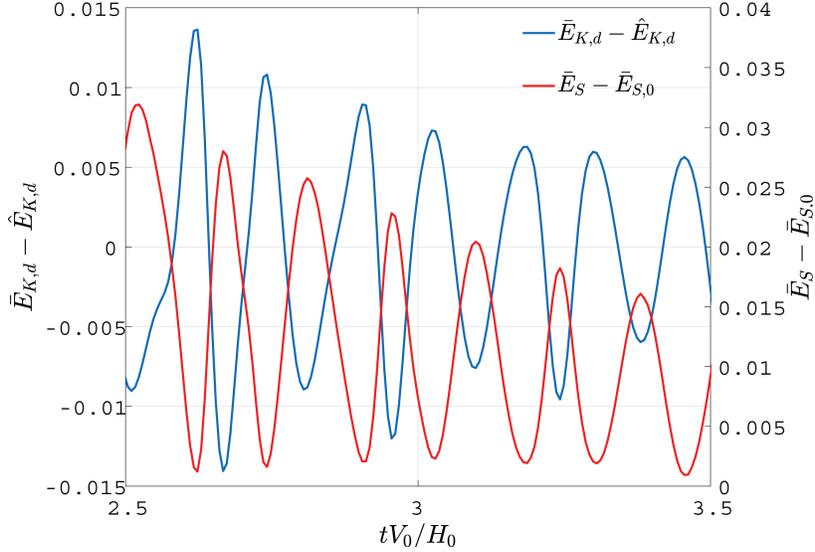


FIG. 5. A close-up view of the fluctuating part of the kinetic and surface energies of the drop after rebound, from figure 3, showing perfect exchange of energies between the two.  $\hat{E}_{K,d}$  represents the moving-average value of the kinetic energy and  $\bar{E}_{S,0}$  is initial surface energy of the drop.

221 near the surface travel azimuthally along the drop's surface amplifying in the process. These waves  
 222 focus at the axis of symmetry resulting in vigorous vertical oscillations of the upper interface of

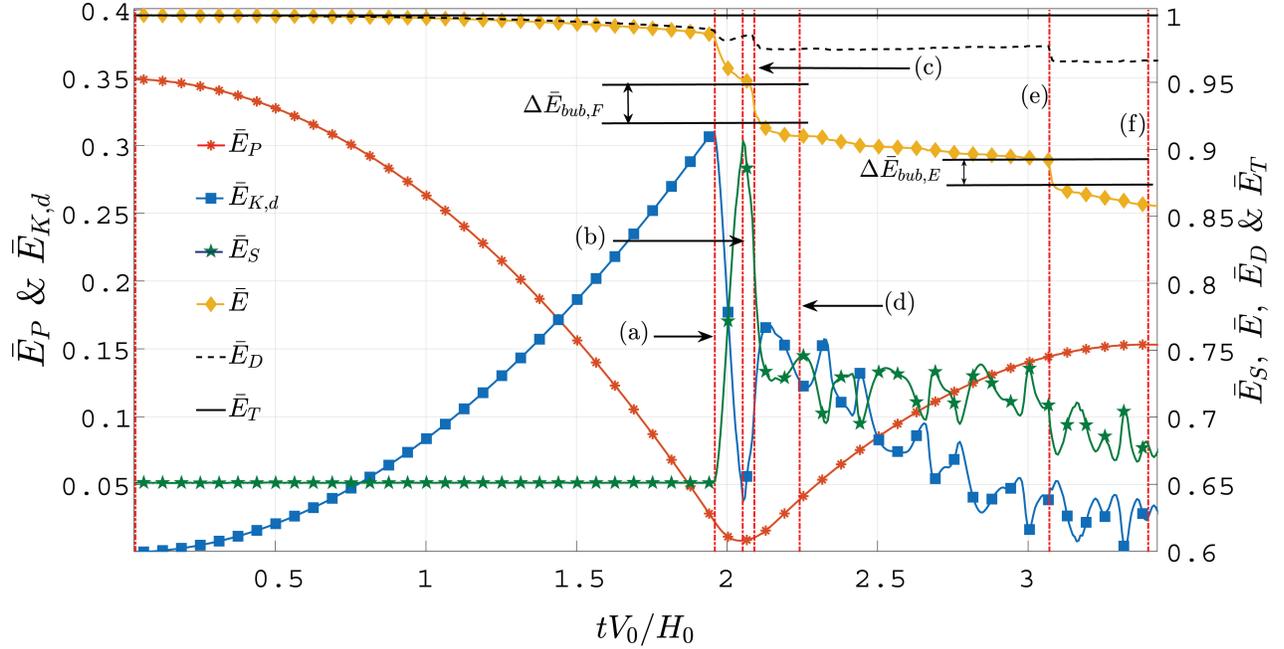


FIG. 6. Energy budget for one complete bouncing cycle for  $We = 3.21$  and  $Re = 1035$  showing various energies associated with the drop and the gas non-dimensionalized with the initial energy  $E_0$ . All quantities are the same as defined in figure 3. The vertical dash-dot lines shown with (a), (b), (c), (d), (e) and (f) represents times at the onset of impact, at maximum deformation of the drop, at the instant of bubble entrapment, at the onset of lift-off, at bubble escape and at maximum height after impact, respectively.

223 the drop as shown in figure 8(a). The interface then descends downwards and undergoes necking.  
 224 This process traps a gas bubble inside it as shown in 8(d). Cusp-like regions are formed at the  
 225 axis of symmetry which results in localised regions of high pressure, figure 7(c). Fluid rapidly  
 226 moves away from this high pressure zones resulting in the formation of a high speed jet. On the  
 227 upper side, the high speed jet breaks up into tiny drops due to rapid acceleration, whereas on the  
 228 lower side, this jet can collide with the trapped bubble generating tiny secondary bubbles inside  
 229 the bubble (see supplementary movie-1). The intense motion results in some of the drop's energy  
 230 to be lost to accelerate the gas, some to viscous dissipation due to rapid and vigorous motions  
 231 inside the drop and a small portion to mass lost from ejection of tiny droplets. This process occurs  
 232 over a very short timescale, shown at time (c), and causes a sudden drop in the drop's energy,  
 233 shown as  $\Delta\bar{E}_{bub,F}$ , which represents the energy lost during bubble entrapment. We show later that  
 234 bubble entrapment and escape result in a sudden increase in viscous dissipation. Figure 9 shows  
 235 the sequence of events leading to trapping of the bubble. Large scale inward motion of the drop

236 as shown in figures 9(a)-(c) shows trapping of a gas bubble inside the drop. Strong vortical flow  
237 is generated inside bubble as revealed in close-up views shown in figures 9(e)-(f) consistent with  
238 the findings of Tripathi *et al.*<sup>26</sup> who noted that vorticity tends to concentrate in the lighter fluid. At  
239 the end of the bubble entrapment process, the upper interface of the drop tends to violently recoil  
240 releasing a high speed jet. Contours of velocity magnitude in figure 9 reveals that significantly  
241 high velocities are generated in the gas phase, particularly after the complete enclosure of the  
242 bubble inside the drop. In physical terms, consider a 1mm water drop impacting a surface with the  
243 same  $We$  as given in figure 9. This translates to impact speed,  $V_0 \approx 0.46m/s$  which leads to gas  
244 velocity of about  $46m/s$ .

247 The trapped bubble remains lodged inside the drop during lift-off at time (d) in figure 6 and  
248 also shown in figure 7(d) and in some cases even stays inside the drop until drop undergoes its  
249 second bounce. In this particular case, the trapped bubble slowly drifts upwards and eventually  
250 emerges out of the drop in a violent escape at time (e). During its emergence, the bubble traps a  
251 thin curved film of liquid between its upper surface and the drop's surface. This thin film ruptures  
252 at its periphery as shown in figure 7(e) similar to the process described in Manica *et al.*<sup>27</sup>. Very  
253 large pressures are generated at the tip of the filament due to tiny curvatures there (see inset of  
254 figure 7(e)). This causes the tip to rapidly retract allowing pressurised gas inside the bubble to  
255 rapidly escape imparting kinetic energy to the gas. Figure 10 shows bubble escape process in finer  
256 detail. A thin film of liquid is trapped between the upper surface of the drop and the escaping  
257 bubble as shown in figure 10a. As soon as the rupture is initiated, pressurised gas inside the  
258 bubble rapidly escapes as evident from the contours of velocity magnitude shown in figure 10(b,c).  
259 Simultaneously, the thin liquid film shown in 10d, now in the form of a filament, rapidly retreats  
260 radially in a time of approximately  $\Delta\bar{t} \approx 8 \times 10^{-4}$ . In dimensional terms, this amounts to a time of  
261 about  $30 \mu s$ . A counter-rotating toroidal vortex pair, figure 10e, is generated in the gas generating  
262 a great deal of viscous dissipation. The retracting filament collapses upon itself resulting in a  
263 vertically accelerating jet (figure 10f) which can hit the drop during its rebound and entrap tiny  
264 gas bubbles again. These tiny secondary bubbles as seen in figure 7(f) may again create tertiary  
265 bubbles, but our simulations do not have sufficient resolution to track escape of these bubbles. See  
266 supplementary movie - 2 to see a 3D visualization of an escaping bubble. The process of bubble  
267 escape causes a sudden drop in the drop's total energy,  $\Delta E_{bub,E}$  as shown at time (e) in figure 6  
268 where the subscript  $E$  denotes an escaping bubble.

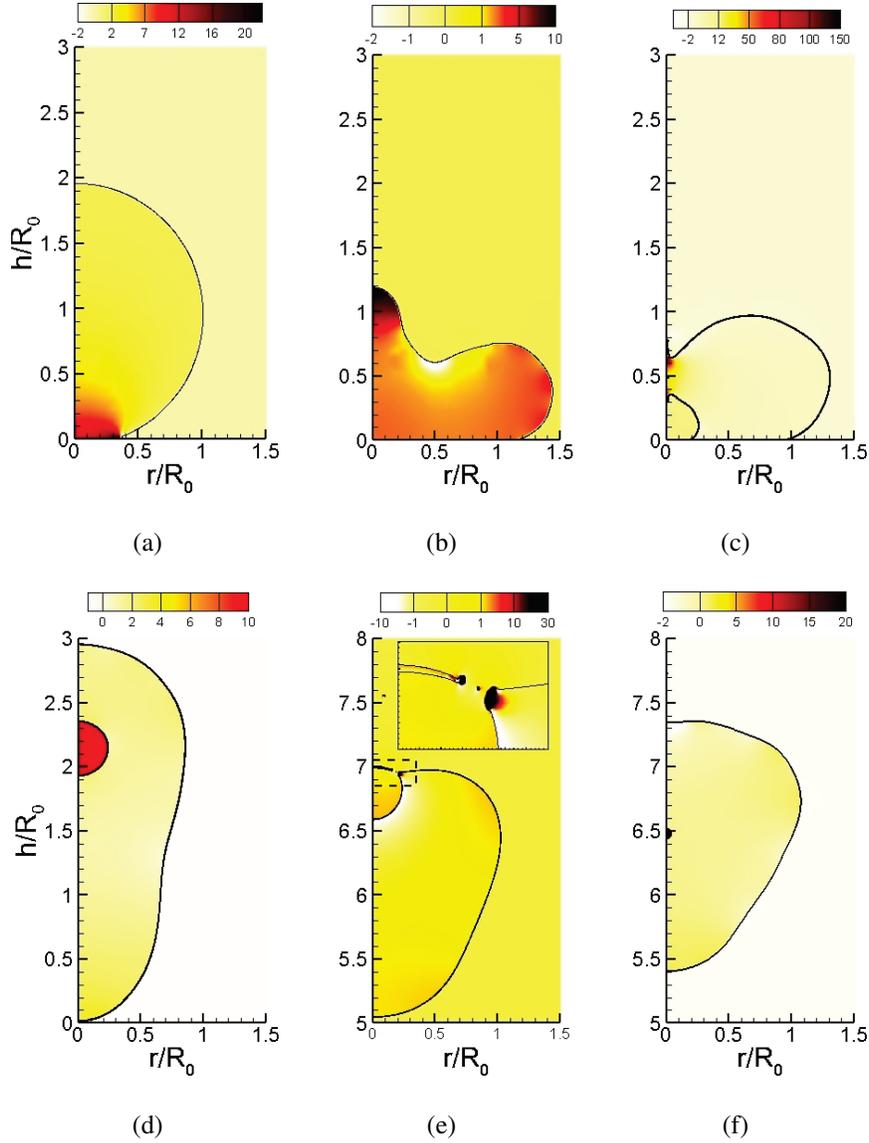


FIG. 7. Drop shapes for  $We = 3.21$  and  $Re = 1035$  at six different times: (a)  $\bar{t} = 1.959$ , (b)  $\bar{t} = 2.047$ , (c)  $\bar{t} = 2.09$ , (d)  $\bar{t} = 2.241$ , (e)  $\bar{t} = 3.071$  and (f)  $\bar{t} = 3.374$ . The colour contours show the variation of non-dimensional pressure,  $\bar{P} = P/(\sigma/R_0)$ . The six panels corresponding to time instants shown with vertical dash-dot lines in the energy budget 6. Note that contour levels are different across the panels. See supplementary online material showing a three-dimensional evolution of bubble entrapment and escape.

## 269 B. Coefficient of restitution

270 In the above discussion, energy budgets were presented for two specific parameter values, viz.,  
 271  $Re = 207, We = 3.21$  and  $Re = 1035, We = 3.21$ . A number of interesting facts emerged from this  
 272 analysis which are briefly listed below: (i) energy loss occurs when the drop is in contact with the

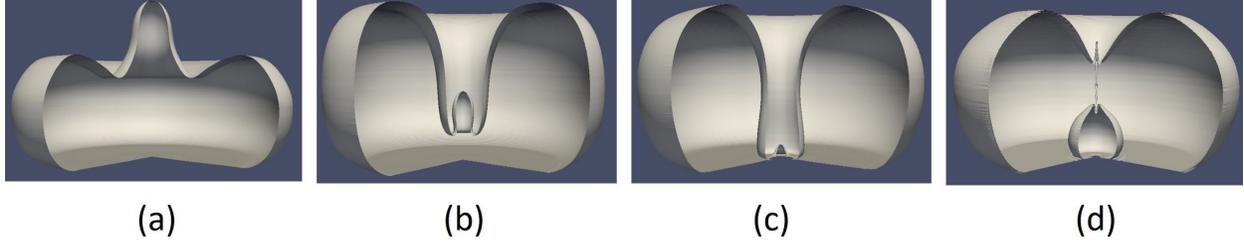


FIG. 8. Three-dimensional representation of drop shapes showing the process of bubble entrapment during drop impact. The four panels are in sequence (from left to right) at non-dimensional time  $\hat{t} = (t - t_0)/\tau$ : (a) 0.82 at maximum spreading, (b) 1.01, at intermediate stage of downward motion of upper interface, (c) 1.06 at the onset of necking of the cylindrical filament, and (d) 1.12, high speed jet ejection at the axis of symmetry, where  $t_0$  is time of first deformation. Parameters used are  $We = 3.21$  and  $Re = 1035$ . See supplementary online material showing a three-dimensional evolution of bubble entrapment.

273 solid surface, (ii) energy loss occurs when the drop is in motion after bouncing from the surface.  
 274 The former occurs primarily due to large shear stresses generated near the solid surface, both in  
 275 the gas and the drop, while the latter occurs due to surface oscillations-induced internal motions  
 276 inside the drop which generates additional viscous dissipation. We estimate both these energy  
 277 losses for the entire range of  $We$  and  $Re$  shown in the phase diagram 2. Conventionally, energy  
 278 loss during impact is represented through the coefficient of restitution defined as

$$279 \quad r_c = \frac{|V_1|}{|V_0|}, \quad (14)$$

280 where  $V_1$  is the velocity after impact and  $V_0$  is the velocity of the drop before impact. In the  
 281 case of a drop which is undergoing large shape changes, velocity is often difficult to determine in  
 282 experiments. In such cases, a height-based coefficient of restitution has sometimes been used:

$$283 \quad r_h = \sqrt{\frac{H_1}{H_0}}, \quad (15)$$

284 where  $H_1$  is the maximum height attained by the drop after the impact and  $H_0$  is the initial release  
 285 height at  $t = 0$ .

286 The two definitions of restitution coefficient will be the same if viscous dissipation in the drop  
 287 during its ballistic motion before and after impact as well as drag from the surrounding gas is  
 288 negligible.

289 De Ruiter *et al.*<sup>15</sup> reported a coefficient of restitution,  $r_c \geq 0.88$  and in some cases, reported  
 290 values as high as  $0.96 \pm 0.04$ . This value is in contrast to the value reported by Kolinski *et al.*<sup>10</sup>

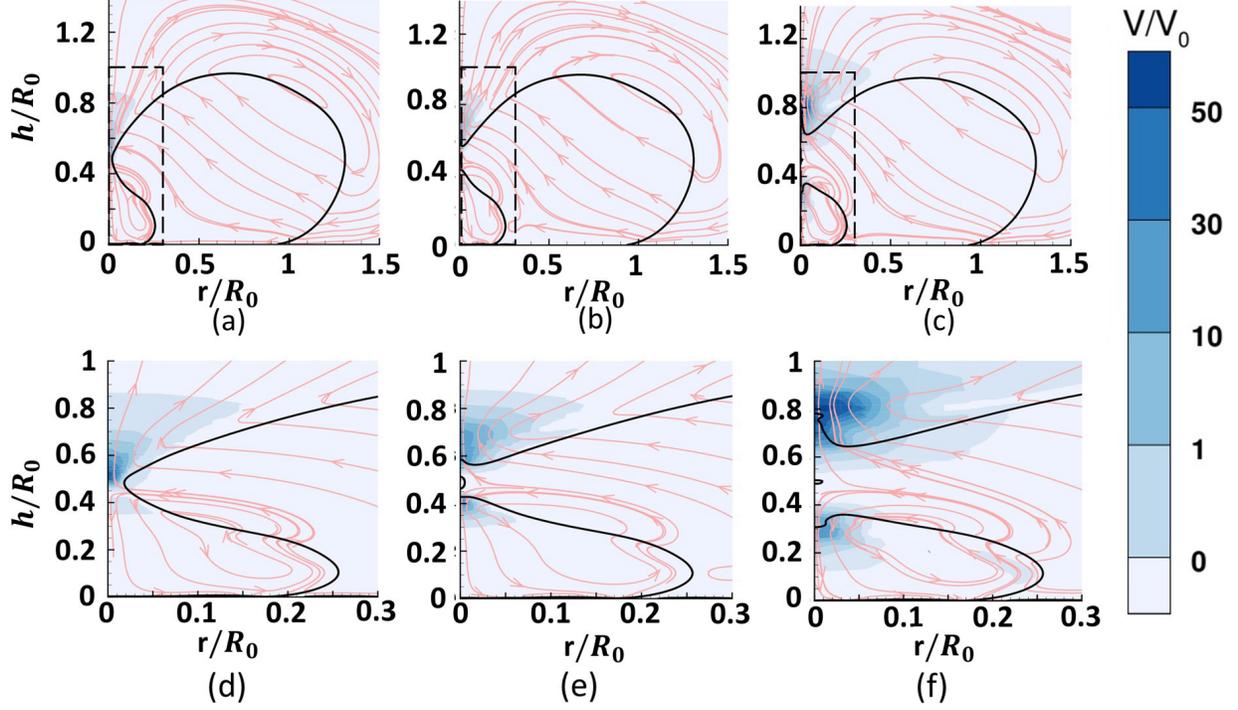


FIG. 9. Flow field during bubble entrapment process for  $We = 3.21$  and  $Re = 1035$  showing instantaneous streamlines and contours of velocity magnitude at (a)  $\bar{t} = 2.0902$ , (b)  $\bar{t} = 2.0904$ , (c)  $\bar{t} = 2.0908$ . Close-up views shown in panels (d), (e) and (f) shows vortical motion inside the trapped bubble. The high speed jet generates intense velocities near the axis of symmetry imparting kinetic energy to the gas and also causes viscous dissipation during bubble entrapment. See supplementary online material showing a three-dimensional evolution of bubble entrapment.

291 who reported  $r_h \leq 0.65$  based on a height-based measurement and it was suggested that such low  
 292 values in  $r_h$  are due to formation of a strong shear-layer in the gas cushion beneath the drop. De  
 293 Ruiter *et al.*<sup>15</sup> use water drops in their experiments whereas Kolinski *et al.*<sup>10</sup> use water-glycerol  
 294 mixtures which increases the viscosity of the drops. Further, the impact velocities are lower in  
 295 the latter case which results in lower  $Re$  values. In both the studies, the surfaces are hydrophilic  
 296 and the drops never make physical contact with the solid surface for the entire range of  $Re$  and  
 297  $We$  considered in the present study. The large variation in the value of restitution coefficient in  
 298 the two studies can be reconciled by examining the role of  $Re$  and  $We$  in these experiments. High  
 299 values of  $r_c$  were also reported in the works of Foote<sup>28</sup> and Richard & Quéré<sup>14</sup>, the former being  
 300 a numerical study for head-on collision of two drops while the latter is an experimental study of  
 301 drops bouncing on superhydrophobic surfaces. De Ruiter *et al.*<sup>15</sup> attributed such high values to

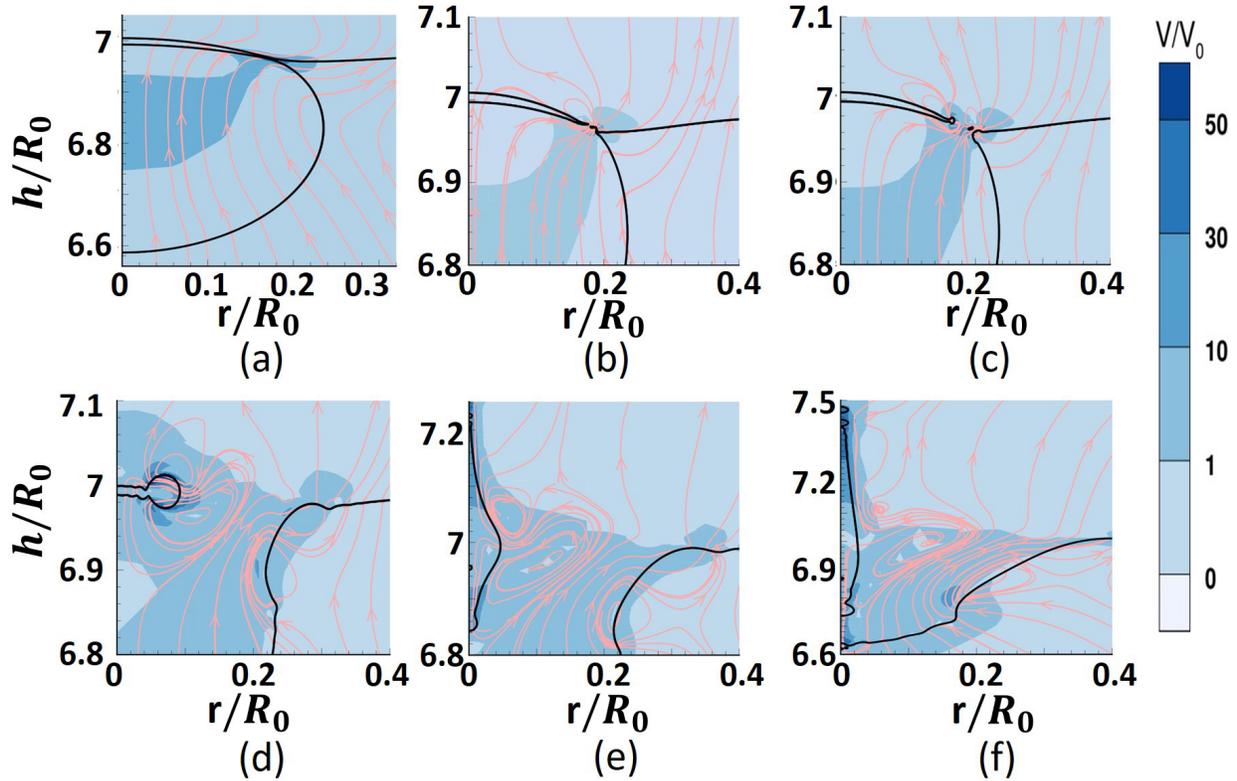


FIG. 10. A close-up view of the fluid motion generated during escape of the entrapped bubble. A thin liquid film trapped between the escaping bubble and the upper surface of the drop ruptures (a,b) and rapidly retreats (c,d). This generates another high speed jet at the axis of symmetry (e,f). The panels are shown in sequence at non-dimensional times,  $\bar{t}$ : (a) 3.0705, (b) 3.071, (c) 3.0711, (d) 3.0718, (e) 3.0724, (f) 3.0737. See supplementary online material showing a three-dimensional evolution of bubble escape.

302 the absence of contact line and the strong repulsion force provided by lubricating gas layer while  
 303 Richard & Quéré<sup>14</sup> attributed high values of  $r_c$  to the low contact time in their experiments. It is  
 304 possible that contact-less bouncing also occurred in Richard & Quéré<sup>14</sup>, but there is no evidence  
 305 of this in their paper. Richard & Quéré<sup>14</sup> suggest that a great deal of energy loss occurs when the  
 306 drop is in flight. By calculating the kinetic energy based on the centre of mass of the drop as well  
 307 as kinetic energy due to internal motions inside the drop, de Ruiter *et al.*<sup>15</sup> obtained a detailed  
 308 energy budget of the drop. Major losses during each bounce was attributed to viscous losses in  
 309 the thin lubricating gas layer. This is consistent with the reason provided by Kolinski *et al.*<sup>10</sup> who  
 310 attributed low  $r_c$  in their experiments to large dissipation in the gas layer.

311 The above survey suggests that viscous losses in the thin intervening gas layer varies as a

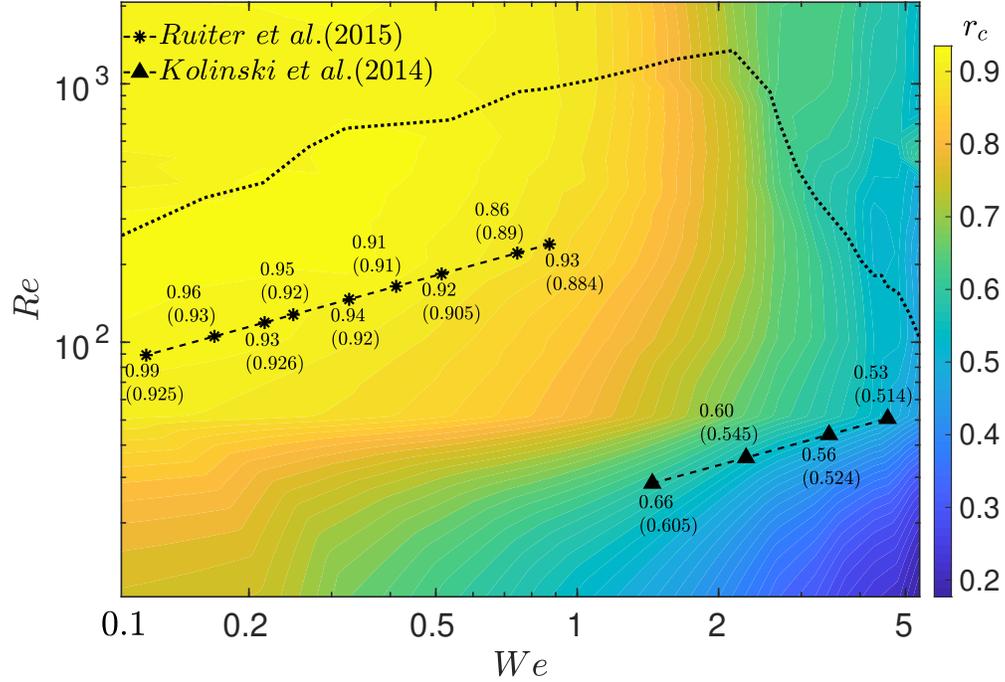


FIG. 11. Variation of coefficient of restitution,  $r_c$ , on the  $We - Re$  plane. The experimental values obtained by de Ruiter *et al.*<sup>15</sup> (water droplet impact on glass) and Kolinski *et al.*<sup>10</sup> (water-glycerol drop on mica) are shown along with simulation shown in brackets. Simulation values are within 10% of the experimentally obtained values.

312 function of  $St$  and  $We$ , where  $St = Re/\lambda$  is the Stokes number and  $\lambda = \mu_g/\mu_l$  is the viscosity ratio.  
313 To reconcile differences between the above studies, we extract the coefficient of restitution  $r_c$  from  
314 our simulation data and plot it in the  $We - Re$  plane as shown in figure 11. The experimental values  
315 of restitution coefficient in de Ruiter *et al.*<sup>15</sup> and Kolinski *et al.*<sup>10</sup> are shown with symbols while  
316 the simulation values at the same  $Re$  and  $We$  are shown alongside in brackets. It is clear that the  
317 agreement with simulations and experiments is satisfactory. More importantly, our simulations  
318 reveal that restitution coefficient strongly varies with both  $Re$  and  $We$ . The differences observed in  
319 the two sets of experiments can thus be attributed to very different experimental parameters used  
320 in the two studies. Figure 11 also reveals that for  $We \gtrsim 1$ ,  $r_c$  becomes less sensitive to Reynolds  
321 number and rapidly decreases with increase in  $We$ . At higher  $We$ , drop undergoes large scale  
322 deformation generating a great deal of vigorous motions inside the drop. This motion coupled  
323 with lower values of surface tension at higher  $We$  causes the drop to spread to greater extent on the  
324 solid surface obeying the scaling law  $r_k \sim We^{1/4}$  where  $r_k$  is the radial extent of the gas layer (see  
325 Sharma & Dixit<sup>13</sup>). This generates a strong shear in the gas layer generating excess dissipation

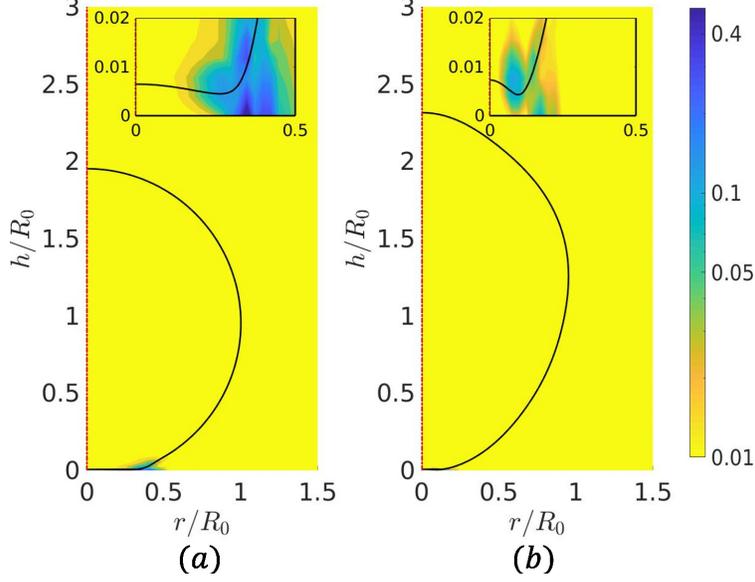


FIG. 12. Contours of non-dimensional rate of dissipation ( $\Phi/\Phi^*$ ) during spreading and receding stages of the drop for  $We = 1.07$  and  $Re = 207$  at (a)  $\hat{t} = 0.19$  and (b)  $\hat{t} = 2.372$ . The inset shows drop-gas interface profile near the solid surface where the rate of dissipation is maximum.

326 at the location of  $h_{min}$ , i.e. where the gas layer is at its thinnest. This can be easily verified by  
 327 determining non-dimensional rate of dissipation written as  $\Phi/\Phi^*$  where  $\Phi$  is given by equn. (8)  
 328 and  $\Phi^*$  is the characteristic value of dissipation. Using impact velocity  $V_0$  and gas layer thickness  
 329 when the drop undergoes its first deformation,  $H_d \sim R_0 Ca_g^{1/2}$ <sup>13</sup>, we have  $\Phi^* = V_0 \sigma / \lambda R_0^2$ . Contours  
 330 of  $\Phi/\Phi^*$  shown in figure 12 at two different times show that dissipation indeed assumes large  
 331 values in the thin gas film, both during spreading and receding stages. Low values of dissipation  
 332 are found inside the drop consistent with the observation in Gopinath & Koch<sup>29</sup> who noted that  
 333 for  $Re \gg We^{1/2}$ , viscous dissipation inside the drop can be neglected.

334 At lower  $We$ , figure 11 shows that  $r_c$  strongly depends on the value of  $Re$  at lower Reynolds  
 335 numbers and weakly depends on Weber number. This is a direct consequence of increased viscos-  
 336 ity at lower  $Re$  which causes large dissipation in the gas film. At low  $We$ , deformation of the drop  
 337 is also reduced, thus  $r_c$  values remain relatively high in this region for a wide range of Reynolds  
 338 numbers as seen in figure 11. The role of  $We$  and  $Re$  becomes even more evident in figure 13 where  
 339 non-dimensional viscous dissipation,  $\bar{D} = D/E_0$  is plotted for four different parameter combina-  
 340 tions. This can be explained using the simple analogy of a mass-spring-damper system given by

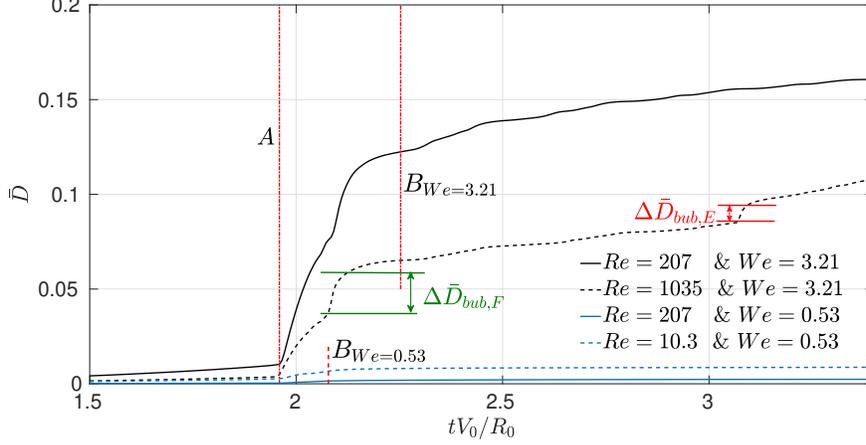


FIG. 13. Variation of non-dimensional viscous dissipation,  $\bar{D} = D/E_0$  for four combinations of  $Re$  and  $We$ . The vertical dash-dot and dashed lines, common for the same value of  $We$ , shows the time instant when contact begins (shown as  $A$ ) and when the drop departs the surface (shown as  $B$ ).

341

342

$$m\ddot{y} + \gamma(We, Re)\dot{y} + k(We)y = F(t), \quad (16)$$

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where damping coefficient  $\gamma$  is a function of both  $Re$  and  $We$  whereas stiffness  $k$  is a function of  $We$  alone. For very low  $We$ , surface tension dominates over inertia and the drop does not exhibit large scale oscillations on its surface. In this limit, the drop largely remains spherical and dissipation/damping simplifies to  $\gamma \approx \gamma(Re)$ . But at higher  $We$ , large scale oscillations inside the drop induces undulations in the underlying gas layer beneath the drop<sup>13</sup>. The radial extent of the gas layer is large at high  $We$  which generates strong shear stress in the gas layer causing viscous dissipation. Further, surface oscillations induced motions contributes to additional viscous dissipation during drop motion in flight.

352

353

The effect of  $We$  and  $Re$  or  $St$  on viscous dissipation can be understood through a simple scaling law derived below. Viscous dissipation during contact given in eqn. (8) scales as

354

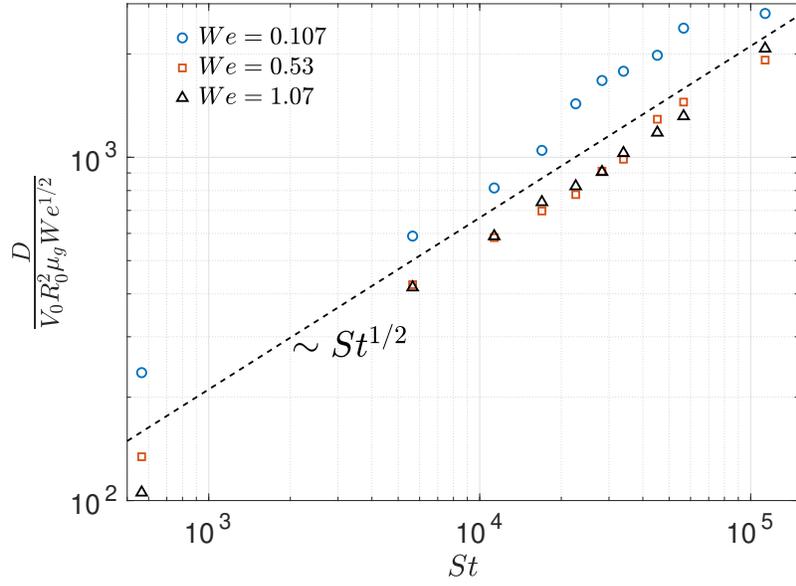
$$D \sim \mu_g \left(\frac{V}{h}\right)^2 \Omega T, \quad (17)$$

355

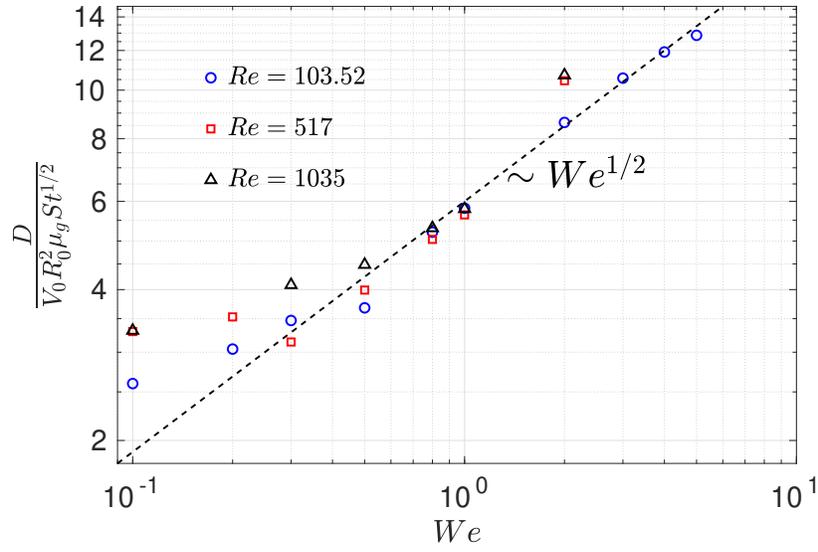
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357

where  $V$  and  $h$  are characteristic velocity and length scales in the gas film,  $\Omega$  is the volume of the gas film beneath the drop and  $T$  is the characteristic time scale. Using impact velocity  $V_0$  for velocity, gas thickness at the drop's first deformation,  $H_d$ , for thickness and inertia-capillary time



(a)



(b)

FIG. 14. Scaling for non-dimensional viscous dissipation as a function of (a) Stokes number, (b) Weber number. The symbols in each plot correspond to three different values of Weber numbers (a) or Reynolds numbers (b). The dashed line shows the scaling law given by equation (19).

358 scale  $\tau \sim (\rho_l R_0^3 / \sigma)^{1/2}$  for time, we have

$$\begin{aligned}
 D &\sim \mu_g \left( \frac{V_0}{H_d} \right)^2 \pi r_k^2 H_d \tau, \\
 &\sim \mu_g \frac{V_0^2}{H_d} r_k^2 \tau
 \end{aligned}
 \tag{18}$$

360 where  $\Omega$  is taken to be the volume of a uniform gas film of thickness  $H_d$  and radius  $r_k$ . In Sharma  
 361 & Dixit<sup>13</sup>, we show that  $H_d \sim R_0 Ca_g^{1/2}$  where  $Ca_g = We/St$  is capillary number based on gas  
 362 viscosity and  $r_k \sim R_0 We^{1/4}$ . Using these expressions, viscous dissipation reduces to

$$D \sim \mu_g V_0 R_0^2 We^{1/2} St^{1/2}.
 \tag{19}$$

364 Figure 14(a) and 14(b) shows variation of non-dimensional viscous dissipation with Stokes number  
 365 (at fixed  $We$ ) and Weber number (at fixed  $St$ ) and the agreement with the scaling law derived  
 366 in equn. (19) is excellent except for low values of  $We$ . Our scaling law derivation makes two  
 367 important assumptions, (i) validity of the lubrication approximation, (ii) time scale  $T \approx \tau$ . At  
 368 very low  $We$ , the extent of the gas film, defined as the radial location of the outer minima in  
 369 gas film thickness, follows the scaling  $r_k \sim R_0 We^{1/4}$ . Hence in the low  $We$  cases, lubrication  
 370 approximation becomes questionable. Following the work of Moláček & Bush<sup>18</sup> who showed  
 371 that, at low  $We$ , time of contact increases with decrease in Weber number, our second assumption  
 372 becomes questionable at low  $We$ . These two reasons explain the deviation of our results in figure  
 373 14(b) from the scaling law (19).

#### 374 IV. ENERGY LOSSES DURING A BOUNCING CYCLE

375 In the previous section, coefficient of restitution was estimated based on the velocities before  
 376 and after impact. Richard & Quéré<sup>14</sup> estimated that most of the energy lost in their experiments  
 377 were due to viscous dissipation during flight. This can occur owing to drag from the surrounding  
 378 gas and internal motions generated inside the drop due to surface oscillations. It is also relevant to  
 379 note that Kolinski *et al.*<sup>10</sup> calculate coefficient of restitution based on maximum drop heights given  
 380 in equn. (15). Large amplitude multi-mode drop oscillations generates large internal circulations  
 381 inside the drop which leads to viscous dissipation which cannot be accounted for in restitution  
 382 coefficient based on change in velocity during impact. In figure 15(a), we first plot the total energy

383 loss,  $L_T = E_0 - E_1$ , that occurs during one complete bouncing cycle, i.e. till the centroid of the  
 384 drop attains a maxima after impact. The contour of energy loss,  $L_T$ , strongly depends on  $We$  as  
 385 evident from the nearly vertical contours. At large  $We$ , energy loss reaches to about 0.4, i.e. 40%  
 386 of drop's energy is lost in one bouncing cycle.

388 To investigate whether this loss occurs during contact or during flight, we plot the ratio of  
 389 energy lost during contact to total energy lost,  $L_c/L_T$ , as shown in figure 15(b). We are primarily  
 390 interested in the wettability-independent region which occurs below the dotted curve in 15(b).  
 391 Consistent with the discussion in the previous section, at high  $We$  energy lost during contact is the  
 392 primary contributor for total energy loss and can be upto 80% of the total loss. At high Weber  
 393 number, which is also the region of interest in Kolinski *et al.*<sup>10</sup>, the drop assumes complex shapes  
 394 generating a great deal of internal motion inside the drop<sup>13</sup>. This results in significant energy loss  
 395 during contact. But at very low  $We$  where the contact time is also very short, most of the energy  
 396 is lost during flight. At  $We \approx 1$ , the loss of energy is nearly equipartitioned between loss during  
 397 contact and loss during flight. Figure 15(b) is one of key findings of this study and establishes  
 398 the role of  $We$  unequivocally on energetics of drop impacts. The patchy region that occurs in the  
 399 wettability-dependent region at high  $Re$  and  $We$  is also the region where bubble entrapment and  
 400 escape occurs. Energy loss during contact in this region depends on the precise nature of bubble  
 401 entrapment process which requires further study.

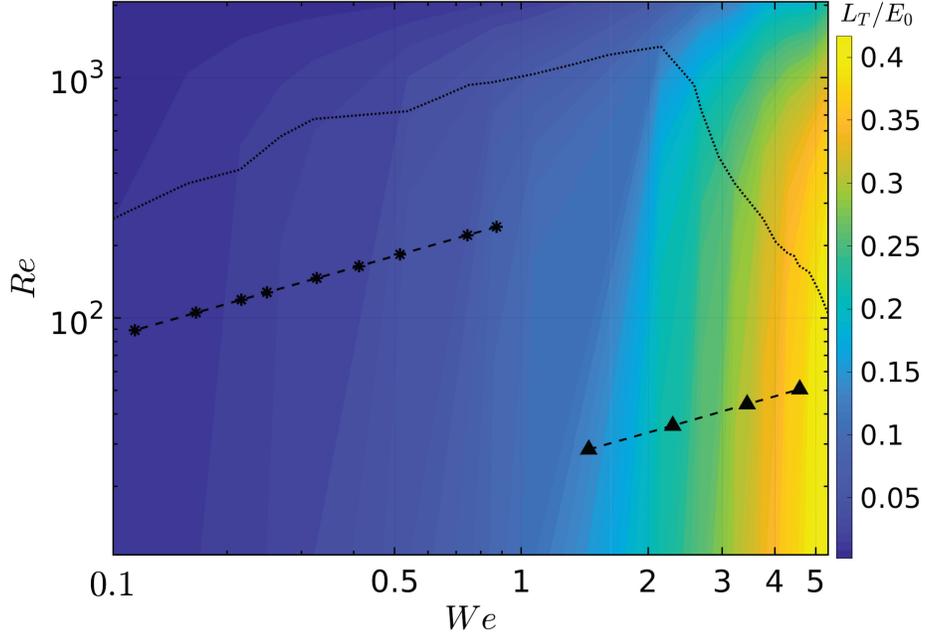
402 The role of Weber number is best illustrated by examining its effect on the drop shape during  
 403 impact. We illustrate this with one specific example taken at  $Re = 51.7$  and at  $We = 2.14, 3.21$ .  
 404 Modal decomposition is carried out by expanding the drop shape in terms of Legendre polynomi-  
 405 als:

$$406 \quad R(t, \theta) = R_0 + \sum_{n=0}^{\infty} c_n(t) P_n(\cos \theta), \quad (20)$$

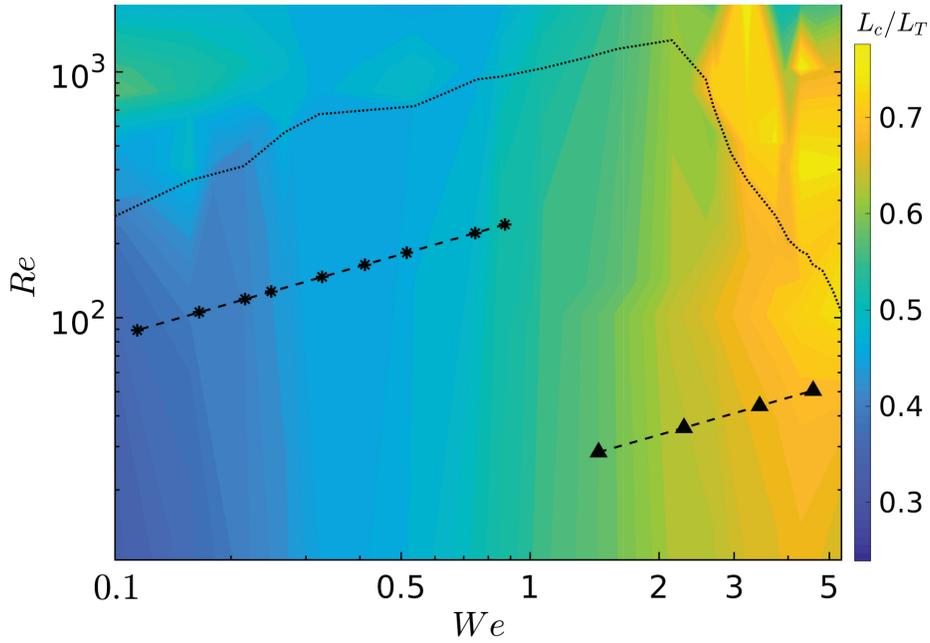
407 where  $n$  is the mode number,  $P_n(\cdot)$  is Legendre polynomial of order  $n$  and  $c_n(t)$  is the corresponding  
 408 coefficient. We use the orthogonality of the Legendre polynomials, to estimate  $c_n$  in terms of drop  
 409 shapes:

$$410 \quad c_n(t) = \frac{2n+1}{2} \int_{-1}^1 (R(t, \theta) - R_0) P_n(\cos \theta) d(\cos \theta). \quad (21)$$

412  
 413 We extract the coefficients  $c_n$  for two different Weber numbers at various times as shown in  
 414 figure 16 for the first 10 modes. At  $We = 0.53$ , dominant surface mode of the drop occurs at  $n = 2$



(a)



(b)

FIG. 15. Variation of (a) energy loss during one complete bouncing cycle,  $L_T/E_0$  and (b) relative contribution of energy loss during contact vis-à-vis total energy loss,  $L_c/L_T$ . Panel (a) shows that maximum energy loss occurs at high Weber numbers and is only weakly dependent on Reynolds number. Panel (b) shows that at higher Weber numbers, contact losses dominate over energy loss that occurs during flight. The symbols correspond to experimental parameters used in de Ruiter *et al.*<sup>15</sup>(\*) and Kolinski *et al.*<sup>10</sup>(▲).

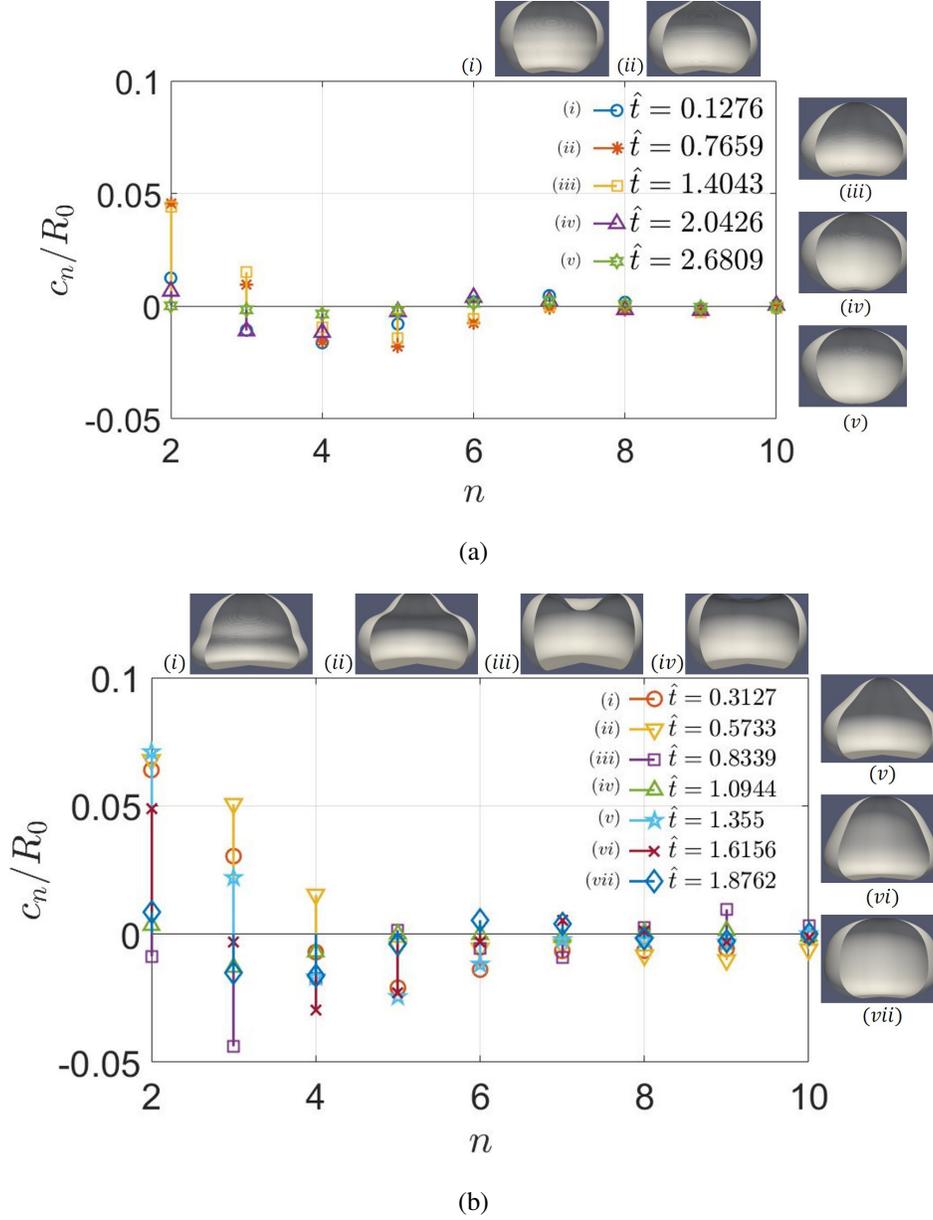


FIG. 16. Modal decomposition for two different cases: (a)  $We = 0.53$ ,  $Re = 51.7$ , (b)  $We = 3.21$ ,  $Re = 51.7$  at various times during drop evolution. For lower values of Weber numbers, the fundamental oscillation mode  $n = 2$  absorbs most of the energy whereas at higher Weber numbers, energy is distributed to higher modes too. Three-dimensional drop shapes shown in each panel correspond to the instants of time when decomposition is carried out.

415 which corresponds to a prolate-oblate shape transition throughout the contact process while higher  
 416 modes have a significantly lower amplitude. But at  $We = 3.21$ , significant energy is transferred  
 417 to higher modes which also leads to faster decay of energy of the drop at this Weber number.

418 Prosperetti<sup>30</sup> studied the viscous decay of an oscillating drop and obtained the decay rate of  
 419 surface oscillations as

$$420 \quad b_0 = (n-1)(2n+1) \frac{\mu_l}{\rho_l R_0^2}. \quad (22)$$

421 This is consistent with the expression for viscous dissipation obtained by Moláček & Bush<sup>18</sup> as-  
 422 suming the flow is approximately irrotational inside the drop:

$$423 \quad D = 8\pi\mu R_0^3 \sum \left( \frac{n-1}{n} \right) c_n^2 \quad (23)$$

424 As one may expect, higher modes indeed decay more rapidly than lower modes as is also found in  
 425 our simulations.

## 426 V. SUMMARY AND CONCLUSIONS

427 In the current work, we present an axisymmetric numerical study of drop impacting a dry solid  
 428 surface. In a related study by Sharma & Dixit<sup>13</sup>, it was shown that drop impact dynamics can  
 429 be divided into a wettability-dependent and wettability-independent regimes depending upon the  
 430 value of Reynolds and Weber number. The present study explores energetics of drop impact with  
 431 the aim of investigating role of Reynolds and Weber numbers on the coefficient of restitution. A  
 432 parametric study is carried out for a wide range of  $Re$  and  $We$  at fixed density and viscosity ratios.  
 433 In each case, potential, kinetic and surface energies as well as viscous dissipation is calculated  
 434 for one complete bouncing cycle. Detailed energy budget is presented for two special cases at  
 435  $We = 3.21$  and  $Re = 207, 1035$  shown in figures 3 and 6. Before impact, surface energy remains  
 436 constant while gravitational potential energy is converted to kinetic energy. Due to low values  
 437 of gas viscosity used in the current study (equivalent of an air-water system), viscous dissipation  
 438 due to drag is negligible. The onset of impact is indicated by a steep rise in surface energy at  
 439 the expense of the drop's kinetic energy until the drop spreads to its maximum radial extent. In  
 440 the wettability-independent bouncing process where the drop is supported on a thin cushion of  
 441 gas, rapid recoil occurs resulting in sharp decline of surface energy. In the wettability-dependent  
 442 process, recoil occurs only for hydrophobic and superhydrophobic surfaces like in the present  
 443 study. Even for such impacts, drop first spreads on a thin gas film sometimes referred to a 'skat-  
 444 ing process'<sup>9</sup> before contact eventually occurs. Strong shear is generated in the gas layer below  
 445 causing a large amount of viscous dissipation. The drop eventually lifts-off completing the contact  
 446 process. The energy loss that occurs during contact,  $L_c$ , is the major contributor in total loss,  $L_T$ ,

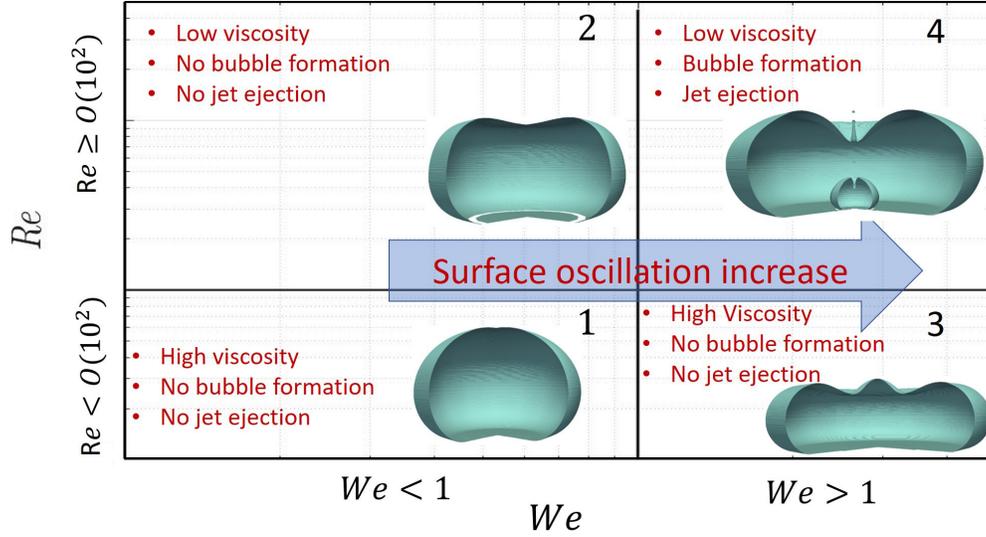


FIG. 17. A schematic view showing various types of drop-solid interactions as a function of  $We$  and  $Re$ . Physical contact with the solid surface occurs at higher values of  $Re$  while surface-oscillations-induces dissipation occurs at higher Weber numbers. Region-4, at higher values of  $We$  and  $Re$ , corresponds to bubble entrapment cases.

447 for high Weber number cases, and is weakly dependent on Reynolds number. Viscous dissipation  
 448 is found to follow a simple scaling law given by  $D \sim \mu_g V_0 R_0^2 We^{1/2} St^{1/2}$ . For high  $We$  and  $Re$ ,  
 449 bubble entrapment can often occur as shown in figures 8 and 9. During this process, drop assumes  
 450 complex shapes and involves ejection of high speed jets causing additional viscous dissipation. As  
 451 the drop rises after contact, strong surface oscillations result in vigorous internal motions inside the  
 452 drop. Such motions cause additional viscous dissipation which can be obtained as  $(L_T - L_c)$ . As  
 453 is clearly evident in figure 15(b), for low  $We$ , bulk of the energy loss occurs during flight whereas  
 454 at high  $We$ , bulk of the energy loss occurs during contact. This is consistent with the experiments  
 455 of Kolinski *et al.*<sup>10</sup> carried out for  $We > 1$  who noted that shear in the gas layer causes bulk of the  
 456 dissipation clearly suggesting the  $L_c$  is the dominant contributor in total energy loss for high  $We$   
 457 impacts.

458 A key result of the paper is a detailed quantification of coefficient of restitution,  $r_c$ , shown in  
 459 figure 11. Low Weber number impacts were found to have a high value of  $r_c$  whereas high Weber  
 460 number impacts were found to have lower values of  $r_c$ . Satisfyingly, the simulations were found  
 461 to be excellent agreement with both Kolinski *et al.*<sup>10</sup> and de Ruiter *et al.*<sup>15</sup>. For the first time, our  
 462 study systematically showed how energetics of a bouncing drop subtly depends on the value of

463 Weber and Reynolds number. The main findings of the paper can be summarised with a simple  
464 schematic shown in figure 17.

465 A number of open questions remain which needs careful experiments and further numerical  
466 studies. Our simulations fail to capture dynamics if gas film thicknesses reach sub-micron lev-  
467 els. For high speed impacts, it is well known that gas films can easily reach nanometer ranges  
468 where both rarefaction as well as non-continuum effects become important. Their role is ener-  
469 getics of impact is unclear and requires further investigation. Our simulations also assume that  
470 the impact, even in wettability-dependent regimes, is axisymmetric, but a number of experiments  
471 have revealed that localised contacts first occur and the subsequent contact line motion is highly  
472 non-axisymmetric. Roughness of the substrate is another important feature which requires further  
473 investigation, mainly with regards to its effect on the coefficient of restitution. Some of these  
474 topics are currently under investigation and will be presented in future studies.

#### 475 **Supplementary Material**

476 See supplementary material showing a three-dimensional evolution of bubble entrapment and es-  
477 cape during drop impact.

#### 478 **AUTHOR'S CONTRIBUTIONS**

479 HND conceptualized, defined the scope and supervised the study, PKS carried out the numeri-  
480 cal computations. HND and PKS analysed the data together. PKS derived the scaling laws and  
481 generated all the figures and movies. HND and PKS wrote the manuscript.

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#### 486 **DATA AVAILABILITY**

487 The data that support the findings of this study are available from the corresponding author upon  
488 reasonable request.

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